Attached is data for Benzene and Toluene and some useful forms of the Peng-Robinson Equation of State. Use this information to determine:

Due: February 20, 2019

1. 10 points

The vapor pressure of pure benzene and toluene at 240°C.

2. 30 points

The fugacity of pure benzene and pure toluene at 240°C and 10 atm total pressure.

3. 30 points

The fugacity of liquid benzene and liquid toluene at 240°C and 30 atm total pressure

4. 30 points

The fugacities of benzene and toluene in a 40/60 mole % mixture when T = 240°C and P=10 atm.

The Peng-Robinson Equation of State:

$$P = \frac{RT}{v - b} - \frac{a}{v(v + b) + b(v - b)}$$

$$\alpha^{0.5} = 1 + \kappa (1 - T_r^{0.5})$$

$$\kappa = 0.37464 + 1.54226\omega - 0.26992\omega^2$$

$$a = \frac{0.45724 R^2 T_c^2 \alpha}{P_c}$$

$$b = \frac{0.07780RT_c}{P_c}$$

also, for shorthand for the P-R equation, use:

$$A = \frac{aP}{R^2T^2}$$

$$B = \frac{bP}{RT}$$

Mixing rules:

$$a = \sum_{i} \sum_{j} y_{i} y_{j} a_{ij}$$

$$b = \sum_{i} y_{i} b_{i}$$

$$a_{ij} = (1 - \delta_{ij})a_i^{0.5}a_j^{0.5}$$

where  $\delta_{ij}$  is an empirical constant for the benzene/toluene mixture:

$$\delta_{ii} = 0$$

$$\delta_{ii} = 0.01$$

Polynomial form:

$$z^3 - (1 - B)z^2 + (A - 3B^2 - 2B)z - (AB - B^2 - B^3) = 0$$

Fugacity coefficient for the mixture:

$$\ln\left(\frac{f_1}{v_1 P}\right) = \ln(\phi_1) =$$

$$\frac{b_1}{b}(z-1) - \ln(z-B) - \frac{A}{2\sqrt{2}B} \left( \frac{2\sum_j y_j a_{1j}}{a} - \frac{b_1}{b} \right) \ln\left( \frac{z+2.414B}{z-0.414B} \right)$$

Fugacity coefficient for the pure component:

$$\ln(f/P) = \ln(\phi) = (z-1) - \ln(z-B) - \left(\frac{A}{2\sqrt{2}B}\right) \ln\left(\frac{z+2.414B}{z-0.414B}\right)$$

Data:

	Benzene	Toluene
MW (g/mole)	78.114	92.141
$T_{c,}K$	562.1	591.7
P <sub>c</sub> , atm	48.3	40.6
$\mathbf{Z}_{\mathrm{c}}$	0.271	0.264
ω	0.212	0.257
constants for Antoine vapor pressure equation		
$\mathbf{A}_1$	-0.3767546E2	-0.2284786E2
$A_2$	-0.1097523E4	-0.1874186E4
$A_3$	-0.9353251E2	-0.7292144E2
$\mathrm{A}_{\scriptscriptstyle{4}}$	-0.14047730E-1	-0.1083663E-1
$A_5$	0.99482220E1	0.7485147E1
$A_6$	0.10416500E-16	0.7567229E-17
$A_7$	6	6

$$\ln(P) = A_1 + \frac{A_2}{T + A_3} + A_4 T + A_5 \ln(T) + A_6 T^{A_7}$$

where:

P is in Pascals

T is in K