

Example Exam

ES 3053 Thermo

EXAM III
Open Books and Notes

November 20, 2019

Name: Solution

A vapor compression refrigeration cycle is used with R-134a working fluid. Use the R-134a table in the appendix of your book for all calculations. Use reasonable assumptions for a typical vapor compression cycle to complete the calculations. However, in this case, there will be a pressure drop in the condenser (usually we assume the condenser is constant P) so that $P_4 = 1400 \text{ kPa}$. The thermal efficiency, η , of the compressor is 75% and the heat load on the evaporator ($\dot{Q}_{\text{evap}}$) is one ton of refrigeration (1 ton = 3.5 kW).

A. 51 points

Fill in the missing numbers in the following table using the numbering sequence given in the figure (each empty box is worth 3 points):

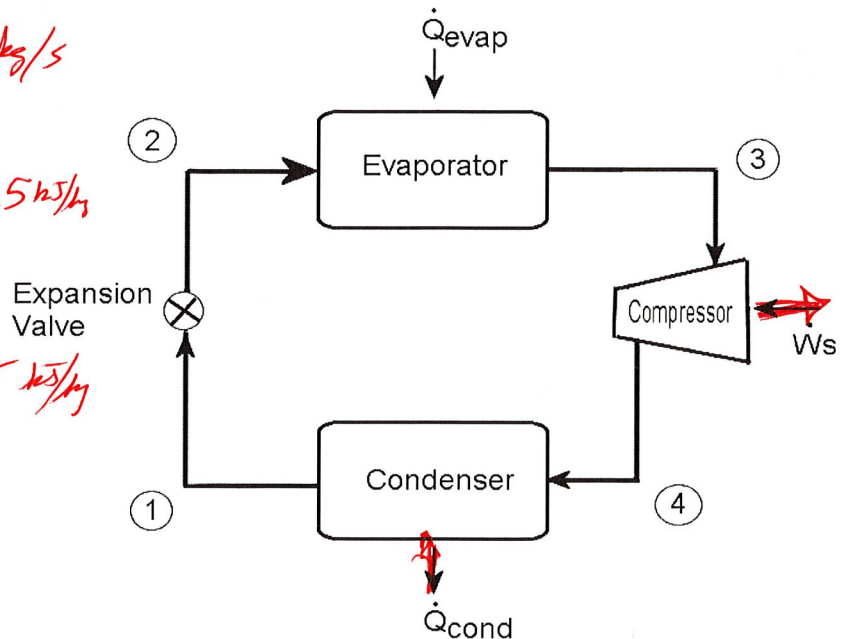
	Point 1	Point 2	Point 3	Point 4' (base case)	Point 4
T (°C)	48	-10	-10	59.7	71.4
P (kPa)	1253.6	200.74	200.74	1400	1400
H (kJ/kg)	120.41	120.41	244.55	285.11	298.63
S (kJ/kg·°K)	0.43251	0.46610	0.93782	0.93782	0.9777
x (vapor fraction)		0.3974			

B. 17 points 0.0282 kg/s

Find the flowrate, $\dot{m}$ of the R-134a

C. 16 points $-\dot{W}_s = 1.525 \text{ kW}$
Find the work requirement for the compressor in kW.

D. 16 points $\dot{Q} = -5.025 \text{ kW}$
Find $\dot{Q}_{\text{cond}}$ in kW.



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Solution

A. Point 1 — sat liquid at 48°C

Point 2 — $H_2 = H_1$, $T = -10^\circ\text{C}$

$$120.41 = (1-x_2)38.53 + x_2(244.55) \quad \text{saturated @ } -10^\circ\text{C}$$

$$x_2 = \frac{0.3974}{0.3974} = 0.3974$$

$$s_2 = 0.3974(0.93782) + (1-0.3974)(0.15496)$$

$$s_2 = 0.46610 \text{ kJ/kg} \cdot \text{K}$$

Point 3, assume sat v @ -10°C

Point 4', $s_4 = s_3 = 0.93782$, $p_4 = 1400 \text{ kPa}$

interpolate between saturated $T = 52.40^\circ\text{C}$ @ $P = 1.4 \text{ MPa} = 1400 \text{ kPa}$

P (MPa) s	h	$T^\circ\text{C}$
0.9107	276.17	52.4
0.93782	<u>285.11</u>	<u>59.7</u>
0.9389	285.47	60.0

$$\text{Point 4: } -W_s' = 285.11 - 244.55 = 40.56$$

$$-W_s = 40.56 / 0.75 = 54.08$$

$$H_4 = 244.55 + 54.08 = 298.63$$

H_4	s_4	T_4
297.10	0.9733	70
298.63	0.9777	71.4
308.34	1.0056	80

B. $\dot{m} \Delta h = \dot{Q} - \dot{W}_s$ across the evaporator

$$\dot{m} (h_1 - h_2) = 3.5 \text{ kJ/s}$$

$$\dot{m} (244.55 - 120.41) = 3.5 \text{ kJ/s}$$

$$\dot{m} = 0.0282 \text{ kg/s}$$

$$C. \quad m \Delta h = \dot{Q} - \dot{W}_s$$

$$(0.0282 \text{ kg/s})(298.63 - 244.55) = -\dot{W}_s$$

$$\boxed{-\dot{W}_s = 1.52473 \text{ kW}}$$

$$D. \quad m \Delta h = \dot{Q} - \dot{W}_s$$

$$(0.0282)(120.41 - 298.63) = \dot{Q}$$

$$\boxed{\dot{Q} = -5.025 \text{ kW}}$$

overall
the cycle

$$m \Delta h = 0 = \dot{Q} + \dot{Q} - \dot{W}_s$$

$$= 3.5 - 5.025 + 1.525 = 0 \quad \checkmark$$