

## Example Exam

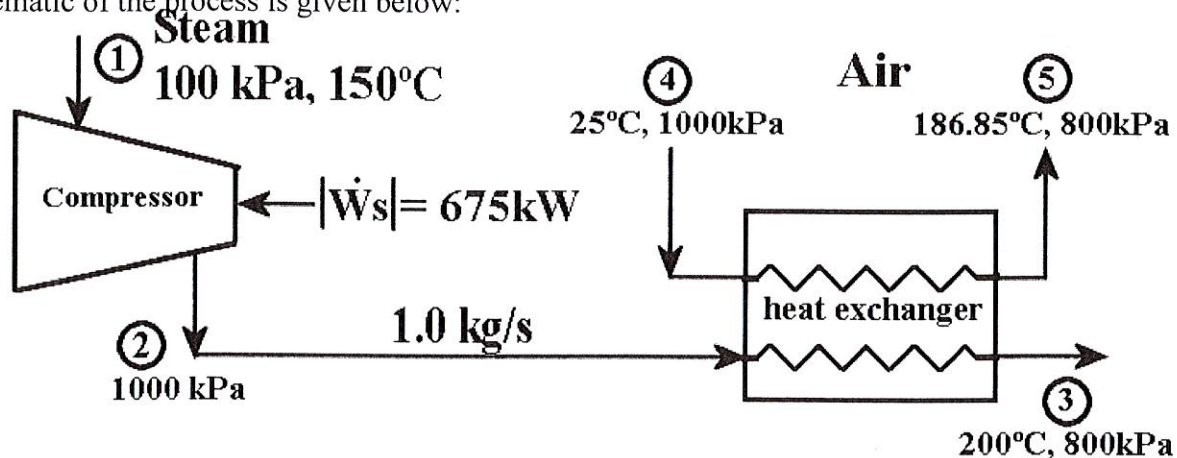
ES 3053

EXAM II  
Open Books and Notes

March 25, 2009

*Solution*

Steam flowing at 1.0 kg/s enters an adiabatic compressor at 150°C and 100kPa (point 1). It is compressed adiabatically to 1000kPa (point 2), requiring 675 kW of power to drive the compressor. The steam then flows to a heat exchanger where it is used to heat a stream of air from 25°C, 1000kPa (point 4) to 186.85°C (460K), 800kPa (point 5). The steam leaves the exchanger at 200 °C and 800kPa (point 3). A schematic of the process is given below:



I. 70 points

Fill in the following table:

|             | Point 1 | Point 2'<br>(isentropic<br>base case) | Point 2<br>(actual case) | Point 3 | Point 4 | Point 5 |
|-------------|---------|---------------------------------------|--------------------------|---------|---------|---------|
| P (kPa)     | 100     | 1000                                  | 1000                     | 800     | 1000    | 800     |
| T (°C)      | 150     | 449.9                                 | 487.4                    | 200     | 25      | 186.85  |
| h (kJ/kg)   | 2776.38 | 3370.98                               | 3451.38                  | 2839.25 | 298.62  | 462.34  |
| s (kJ/kg-K) | 7.6133  | 7.6133                                | 7.7247                   | 6.8158  | 6.2022  | 6.7076  |

II. 15 points

Find the thermal efficiency,  $\eta$ , of the compressor.

$\eta = 0.881$

III. 15 points

Find the flowrate of air assuming there is no heat loss from the heat exchanger.

$\dot{m}_{air} = 3.74$  kg/s

Instructions:

1. Use the steam table, Table B.1, beginning on page 510 of your textbook for steam properties.
2. Use the ideal-gas properties of air given in Table A7.1 on page 496 of your text for air properties.
3. Turn in your calculations with this sheet filled in. Failure to turn in your calculations will result in no credit for the problem.

Solution

I.  $\boxed{\begin{aligned} h_1(100 \text{ kPa}, 150^\circ\text{C}) &= 2776.38 \text{ kJ/kg} \\ s_1(100 \text{ kPa}, 150^\circ\text{C}) &= 7.6133 \text{ kJ/kg}\cdot\text{K} \end{aligned}}$

interpolate here are:

| $T$ | $s$    | $h$     |
|-----|--------|---------|
| 400 | 7.4650 | 3263.88 |
| ?   | 7.6133 | ?       |
| 500 | 7.7621 | 3478.44 |

$\boxed{\begin{aligned} T_2' &= 449.9 \\ h_2' &= 3370.98 \end{aligned}}$

$\Delta h' = 3370.98 - 2776.38 = 594.6 \text{ kJ/kg}$   
 $\Delta h(\text{actual}) = \frac{594.6}{0.881} = 675 \text{ kJ/kg}$

Point 2 actual case

$(h_2 - 2776.38) 1 \text{ kg/sec} = 675 \text{ kJ/sec}$

$\boxed{h_2 = 2776.38 + 675 \text{ kJ/kg} = 3451.38 \text{ kJ/kg}}$

| $T$ | $h$     | $s$    |
|-----|---------|--------|
| 400 | 3263.88 | 7.4650 |
| ?   | 3451.38 | ?      |
| 500 | 3478.44 | 7.7621 |

$\boxed{\begin{aligned} s_2 &= 7.7247 \\ T_c &= 487.4 \end{aligned}}$

Point 3

$\boxed{\begin{aligned} s(800 \text{ kPa}, 200^\circ\text{C}) &= 6.8158 \\ h(800 \text{ kPa}, 200^\circ\text{C}) &= 2839.25 \end{aligned}}$

For air, point 4

$h(1000 \text{ kPa}, 25^\circ\text{C}) = 298.62 \text{ kJ/kg}$

$s(1000 \text{ kPa}, 25^\circ\text{C}) = 6.86305 \text{ kJ/kg}\cdot\text{K} - \frac{0.287}{1.004} \ln \frac{1000}{100} = 6.2022 \text{ kJ/kg}\cdot\text{K}$

For air, point 5

$h(800 \text{ kPa}, 460\text{K}) = 462.34 \text{ kJ/kg}$

$s(800 \text{ kPa}, 460\text{K}) = 7.30142 \text{ kJ/kg}\cdot\text{K} - \frac{0.287}{1.004} \ln \frac{800}{100} = 6.7046 \text{ kJ/kg}\cdot\text{K}$

$s(800 \text{ kPa}, 460\text{K}) = 6.7046 \text{ kJ/kg}\cdot\text{K}$

$\frac{0.287}{1.004} \ln \frac{800}{100} = 0.287 \ln \frac{800}{100} = 0.287 \ln 8 = 0.287 \times 2.079 = 0.597$

II.  $\boxed{\eta = \frac{3370.98 - 2776.38}{675} = 0.881}$

III.  $(1 \text{ kg/sec})(675 \text{ kJ/kg}) = \dot{m}_{\text{air}}(462.34 - 298.62) \text{ kJ/kg}$   
 $\dot{m}_{\text{AIR}} = 3.74 \text{ kg/sec}$