

Use the Peng-Robinson Equation of State and data in the back of S&VNAS 8th ed. to determine:

1. 10 points

The vapor pressure of pure chloroform (1) and cyclohexane (2) at 225°C in bar.

2. 30 points

The fugacity (in bar) of pure chloroform and pure cyclohexane at 225°C and 10 bar total pressure.

3. 30 points

The fugacity (in bar) of pure liquid chloroform and pure liquid cyclohexane at 225°C and 40 bar total pressure. The molar volume of pure liquid chloroform is 85.63 cm³/mole and of cyclohexane is 108.16 cm³/mole.

4. 30 points

The fugacities (in bar) of chloroform and cyclohexane in a 40/60 mole % mixture when T = 225°C and P = 10 bar.

Instructions for submitting the project:

1. Use Excel to solve the problem. *Each student should start with a blank worksheet in preparing their solution. Starting with another student's work or work you get elsewhere (such as the internet) is an act of academic dishonesty.*
2. **Using the hardcopy template (or a similar sheet) which is attached, turn in a paper solution. Your Excel sheet should parallel your hardcopy solution.** Be sure to include comments on the Excel sheet and include references to the parts of the problem you are working.
3. Save the Excel sheet as "Project1-FirstName-LastName.xlsx" and email it to me *before* class the date it is due with the subject line: "ChE3063 Project 1 Solution". Submit your paper solution at the beginning of class the date it is due. It should be folded lengthwise with your name on the outside just like homework.

The Peng-Robinson Equation of State:

$$P = \frac{RT}{v - b} - \frac{a}{v(v + b) + b(v - b)}$$

$$\alpha^{0.5} = 1 + \kappa(1 - T_r^{0.5})$$

$$\kappa = 0.37464 + 1.54226\omega - 0.26992\omega^2$$

$$a = \frac{0.45724R^2 T_c^2 \alpha}{P_c}$$

$$b = \frac{0.07780RT_c}{P_c}$$

also, for shorthand for the P-R equation, use:

$$A = \frac{aP}{R^2 T^2}$$

$$B = \frac{bP}{RT}$$

Mixing rules:

$$a = \sum_i \sum_j y_i y_j a_{ij}$$

$$b = \sum_i y_i b_i$$

$$a_{ij} = (1 - \delta_{ij}) a_i^{0.5} a_j^{0.5}$$

where δ_{ij} is an empirical constant for the chloroform/cyclohexane mixture:

$$\delta_{ii} = 0$$

$$\delta_{ij} = 0.01$$

Polynomial form:

$$z^3 - (1 - B)z^2 + (A - 3B^2 - 2B)z - (AB - B^2 - B^3) = 0$$

Fugacity coefficient for the first component in a mixture of j components:

$$\ln\left(\frac{f_1}{y_1 P}\right) = \ln(\phi_1) =$$

$$\frac{b_1}{b}(z - 1) - \ln(z - B) - \frac{A}{2\sqrt{2}B} \left(\frac{2\sum_j y_j a_{1j}}{a} - \frac{b_1}{b} \right) \ln\left(\frac{z + 2.414B}{z - 0.414B}\right)$$

Note that z in the above equation is the compressibility factor for the mixture.

Fugacity coefficient for a pure component:

$$\ln(f / P) = \ln(\phi) = (z - 1) - \ln(z - B) - \left(\frac{A}{2\sqrt{2}B} \right) \ln\left(\frac{z + 2.414B}{z - 0.414B} \right)$$

Hardcopy Template

1. The vapor pressure of pure chloroform and cyclohexane at 225°C in bar

$P_1^S = \underline{\hspace{2cm}}$ bar ; $P_2^S = \underline{\hspace{2cm}}$ bar

2. The fugacity (in bar) of pure chloroform and pure cyclohexane at 225°C and 10 bar total pressure

	Chloroform	Cyclohexane
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T_r
 P_r
 α
 κ
 a
 b
 A
 B
 z
 ϕ
 f (fugacity)

3. The fugacity (in bar) of pure liquid chloroform and pure liquid cyclohexane at 225°C and 40 bar total pressure

	Chloroform	Cyclohexane
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T_r
 P_r
 α
 κ
 a
 b
 A
 B
 z
 ϕ_i^S
 f (fugacity)

4. The fugacities (in bar) of chloroform and cyclohexane in a 40/60 mole % mixture when $T = 225^\circ\text{C}$ and $P = 10$ bar.

	Chloroform	Cyclohexane
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T_r
 P_r
 α
 κ
 a (mixture)
 b (mixture)
 A (mixture)
 B (mixture)
 z (mixture)
 ϕ
 f (fugacity)

